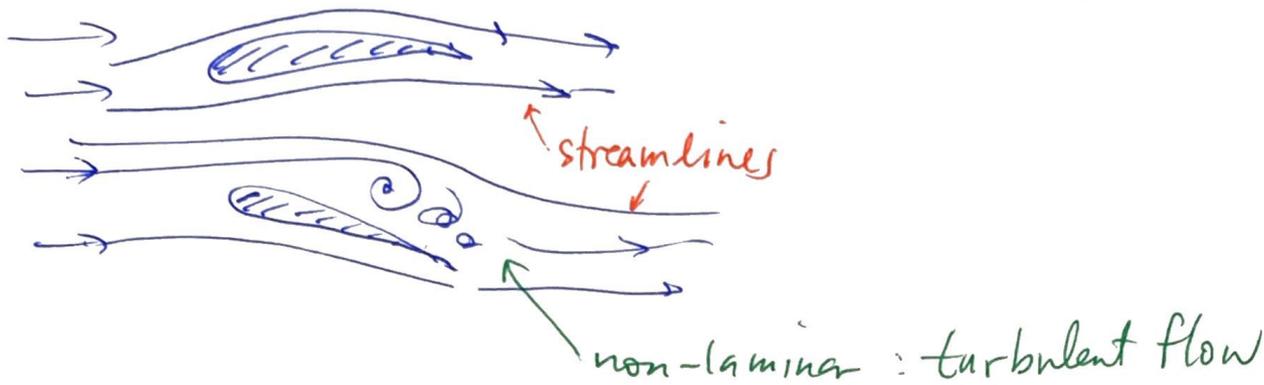


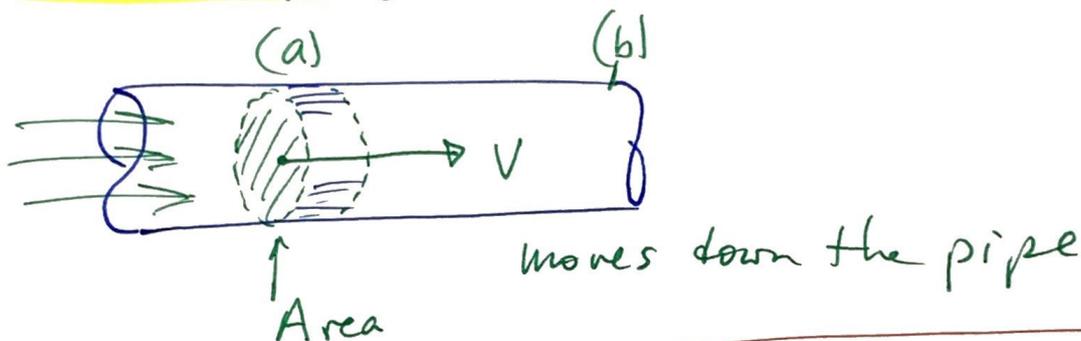
# 106 Fluid Dynamics

①

We study laminar fluid flow. In this type of flow the particles of liquid stay near by each other.



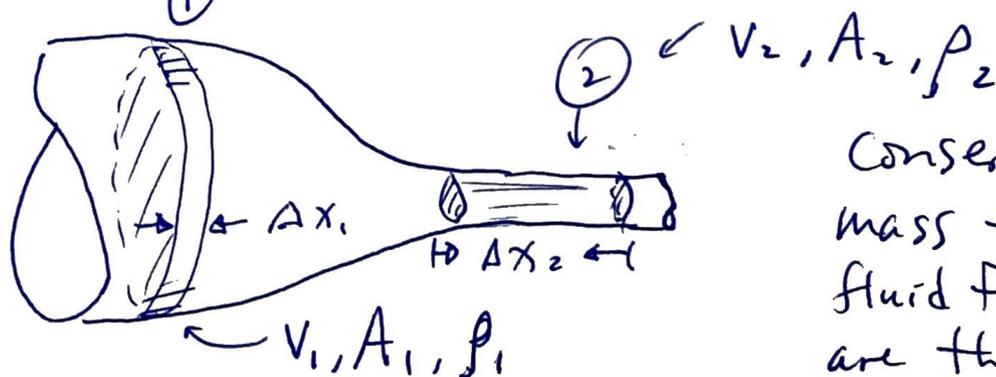
## \* mass flow rate



at station (a)  $\left. \text{mass flow rate} \right|_a = \frac{\text{mass of the "puck" of water}}{\text{change in time}}$

$$\text{flow rate} = \frac{\Delta \text{mass}}{\Delta t}$$

\* If the pipe narrows then the "puck" changes shape



Conservation of mass tells us that fluid flow rates are the same...

Flow rate at 1 = rate at 2

$$\frac{\Delta m_1}{\Delta t} = \frac{\Delta m_2}{\Delta t}$$

$$\frac{\rho_1 V_1}{\Delta t} = \frac{\rho_2 V_2}{\Delta t} \quad \Rightarrow V = A \cdot \Delta x$$

$$\frac{\rho_1 A_1 \Delta x_1}{\Delta t} = \frac{\rho_2 A_2 \Delta x_2}{\Delta t} \quad v_1 \quad v_2$$

$$\rho_1 A_1 v_1 = \rho_2 A_2 v_2$$

mass flow rate  
eqn  
compressible flow

• Incompressible  $\rho_1 = \rho_2$

Then the flow rate becomes

$$A_1 v_1 = A_2 v_2$$

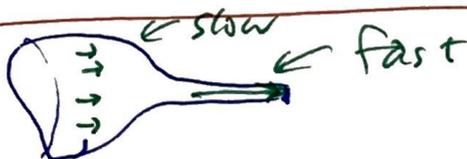
⊗ Application

• IF  $A_1 > A_2$  then  $\frac{A_1}{A_2} > 1$  so

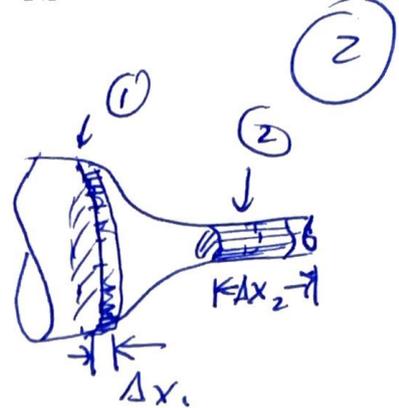
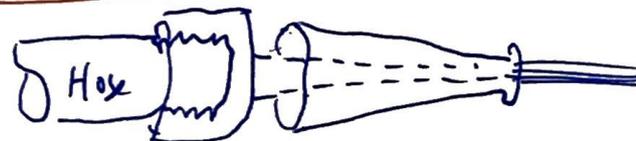
$$v_2 = \left( \frac{A_1}{A_2} \right) v_1$$

shows us that  $v_2 > v_1$

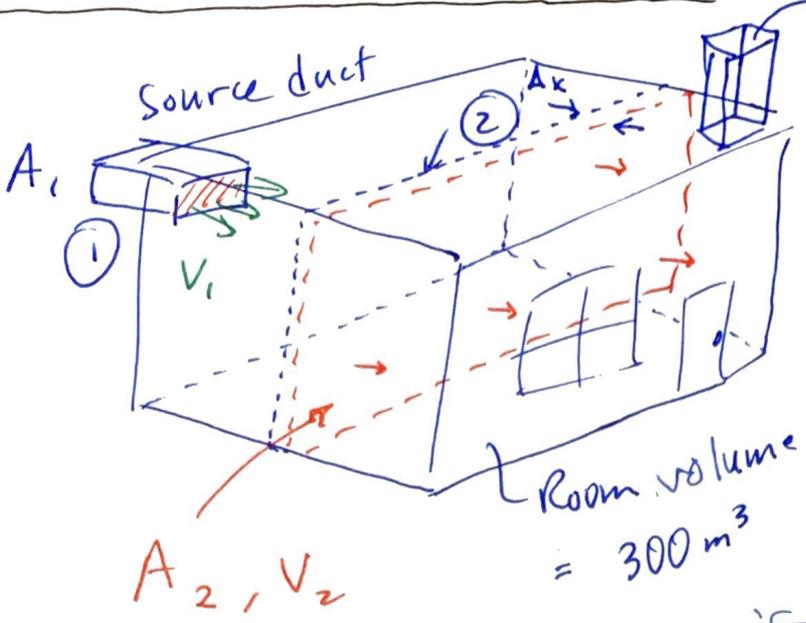
Narrow cross-sectional area has faster flow



EX



EX



return duct

3

Q: what area of duct is need to replenish the air in the room every 15 minutes

if  $v_1 = 3\text{m/s}$  is duct flow?

rate @ 1 = rate @ 2

$$\rho_1 A_1 v_1 = \rho_2 A_2 v_2$$

incompressible flow

$$A_1 v_1 = A_2 v_2$$

$v = \frac{\Delta x}{\Delta t}$   $\rho_1 = \rho_2$

$$A_1 v_1 = A_2 \frac{\Delta x}{\Delta t}$$

$A_2 \Delta x = \Delta \text{Vol.}$

$$A_1 v_1 = \frac{V_2}{\Delta t}$$

← volume of Room

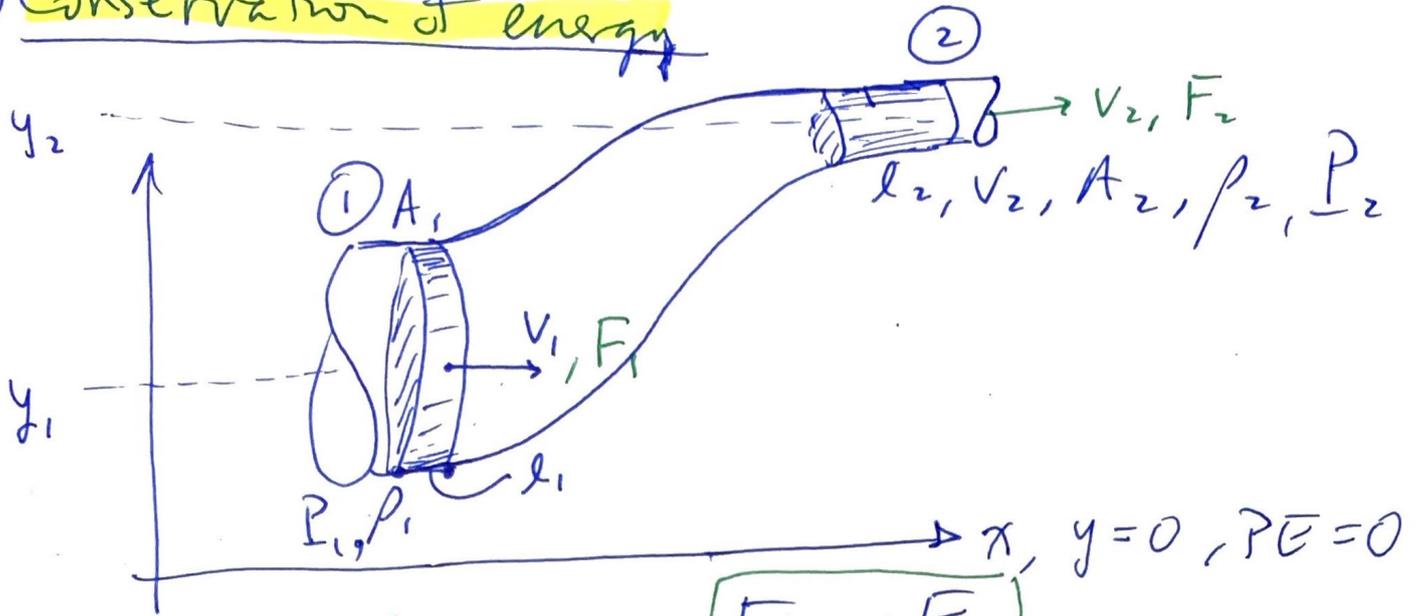
$$\Rightarrow A_1 = \frac{V_2}{v_1 \Delta t} = \frac{300 \text{ m}^3}{(3 \text{ m/s})(15 \text{ min}) \left( \frac{60 \text{ s}}{\text{min}} \right)}$$

$$A_1 = 0.11 \text{ m}^2$$

1/10 of the size of the dish washer box.

# ⊛ Conservation of energy

(4)



## • Conservation of energy

$$E_1 = E_2$$

$$\text{OR } \Delta W @ 1 + KE @ 1 + PE @ 1 = \Delta W @ 2 + KE @ 2 + PE @ 2$$

$$F_1 \cdot l_1 + \frac{1}{2} m_1 v_1^2 + m_1 g y_1 = F_2 \cdot l_2 + \frac{1}{2} m_2 v_2^2 + m_2 g y_2$$

$$(P_1 A_1) l_1 + \frac{1}{2} \rho_1 V_1 v_1^2 + \rho_1 V_1 g y_1 = P_2 A_2 l_2 + \frac{1}{2} \rho_2 V_2 v_2^2 + \rho_2 V_2 g y_2$$

let  $A_1 l_1$  and  $A_2 l_2$ , factor out

$$\underline{A_1 l_1} [P_1 + \frac{1}{2} \rho_1 v_1^2 + \rho_1 g y_1] = \underline{A_2 l_2} [P_2 + \frac{1}{2} \rho_2 v_2^2 + \rho_2 g y_2]$$

• use conservation of mass flow  $\underline{A_1 l_1 = A_2 l_2}$

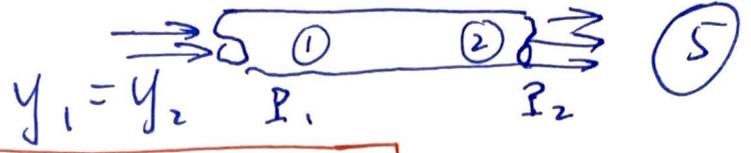
$$\underline{P_1 + \frac{1}{2} \rho_1 v_1^2 + \rho_1 g y_1 = P_2 + \frac{1}{2} \rho_2 v_2^2 + \rho_2 g y_2}$$

Bernoulli's Equation : Cons. of energy .

$$\Rightarrow \underline{P + \frac{1}{2} \rho v^2 + \rho y g = \text{constant}}$$

# Applications

• level pipe flow



$$y_1 = y_2$$

$$P_1 + \frac{1}{2} \rho_1 v_1^2 = \frac{1}{2} \rho_2 v_2^2 + P_2$$

• multi height pipe but **no flow**  $v_1 = 0, v_2 = 0$   
 • incompressible  
 • "slow"

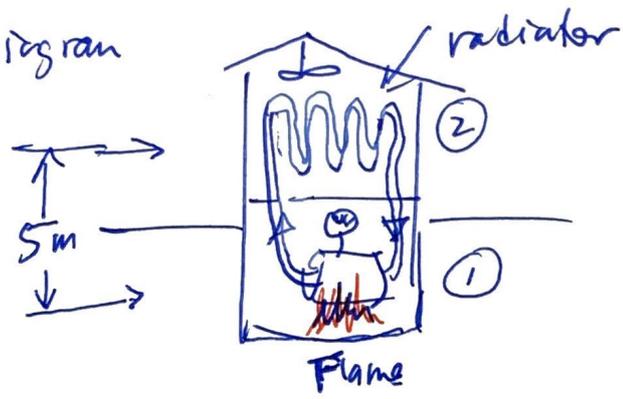
$$\Delta P = \rho g \Delta y$$

This is just hydrostatic pressures seen in 10a  $P = \rho g h$

Ex

Consider a hot water radiative heating in an older house

(i) Diagram



Water is pumped through the hot water pipe at 0.5 m/s and the pipe is 4.0 cm in diameter. The boiler runs at 3.0 atm.

Q: what will be the speed and pressure on the second floor if the pipe diameter narrows to 2.6 cm. Assume 5 meters between boiler and radiator.

Variables @ (1)

$$\begin{cases} v_1 = 0.5 \text{ m/s} \\ r_1 = 2 \text{ cm} \\ P_1 = 3 \text{ atm} \\ y_1 = 0 \end{cases}$$

Variables @ (2)

$$\begin{cases} v_2 = ? \\ r_2 = 1.3 \text{ cm} \\ P_2 = ? \\ y_2 = 5 \text{ m} \end{cases}$$

Cont. ↓

Cont. Assume incompressible  $\rho_1 = \rho_2$   
 Ex. We have one eqn and two unknowns (6)

Bernie's Eqn  $\left\{ \begin{aligned} P_1 + \frac{1}{2} \rho_1 v_1^2 + \rho_1 y_1 g &= P_2 + \frac{1}{2} \rho_2 v_2^2 + \rho_2 y_2 g \\ &\quad \uparrow ? \quad \quad \quad \uparrow ? \end{aligned} \right.$

mass flow  $\left\{ \begin{aligned} \rho_1 v_1 A_1 &= \rho_2 v_2 A_2 & \rho_1 = \rho_2 &= \rho_{H_2O} \end{aligned} \right.$

$$\Rightarrow v_2 = \left( \frac{A_1}{A_2} \right) v_1 = \left( \frac{2 \text{ cm}}{1.3 \text{ cm}} \right)^2 (0.5 \text{ m/s})$$

$$= \left( \frac{\pi r_1^2}{\pi r_2^2} \right) v_1 \quad \boxed{v_2 = 1.2 \text{ m/s}}$$

Insert this into Bernoulli's eqn:

$$P_1 + \frac{1}{2} \rho v_1^2 + \rho g y_1 = P_2 + \frac{1}{2} \rho v_2^2 + \rho g y_2$$

$$P_1 + \frac{1}{2} \rho (v_1^2 - v_2^2) + \rho g \underbrace{(y_1 - y_2)}_{\Delta y} = P_2$$

$$\left( 3 \times 1.01 \times 10^5 \frac{\text{N}}{\text{m}^2} \right) + \frac{1}{2} \left( 10^3 \frac{\text{kg}}{\text{m}^3} \right) \left[ (0.5 \frac{\text{m}}{\text{s}})^2 - (1.2 \text{ m/s})^2 \right] + \left( 10^3 \frac{\text{kg}}{\text{m}^3} \right) [0 - 5 \text{ m}]$$

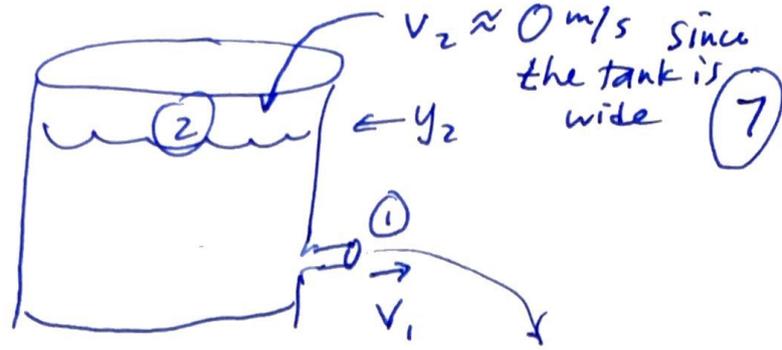
$$= P_2$$

$$P_2 = 2.5 \times 10^5 \frac{\text{N}}{\text{m}^2} \quad \text{or} \quad \boxed{2.5 \text{ atm}}$$

- Higher altitude
- narrow pipe
- Faster Flow
- Lower pressure

# Applications

## Torricelli Flow



Since both top & pipe are exposed to the air we will let  $P_1 = P_2$

Bernoulli's

$$P_1 + \frac{1}{2} \rho v_1^2 + \rho g y_1 = P_2 + \frac{1}{2} \rho v_2^2 + \rho g y_2$$

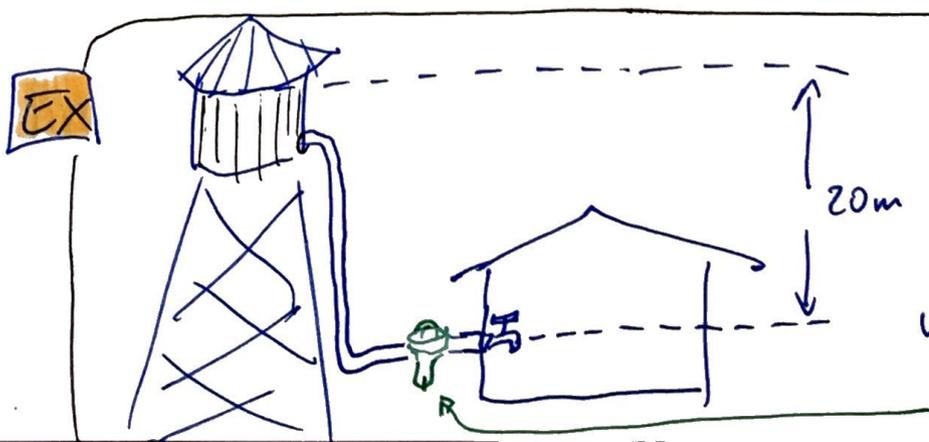
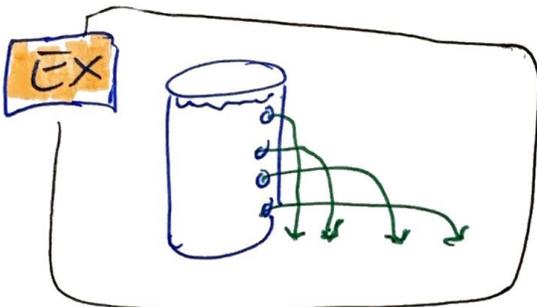
Bottom Top

$$\frac{1}{2} \rho v_1^2 = \rho g y_2 - \rho g y_1$$

$$v_1 = \sqrt{2g(y_2 - y_1)}$$

Torricelli's eqn.

Recall  
In Chpt 6 :  $\frac{1}{2} m v^2 = m g h \rightarrow v = \sqrt{2gh}$

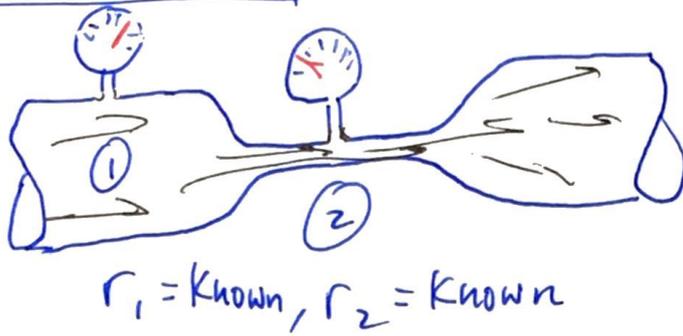


$$v_1 = \sqrt{2(9.8)(20m)}$$

$$v_1 = 19.8 \text{ m/s such!}$$

we need a pressure regulator

- Venturi Flow Meter : Find flow speed in a pipe. (8)



By measuring  $P_2, P_1$   
we can  
calculate  $v_1$

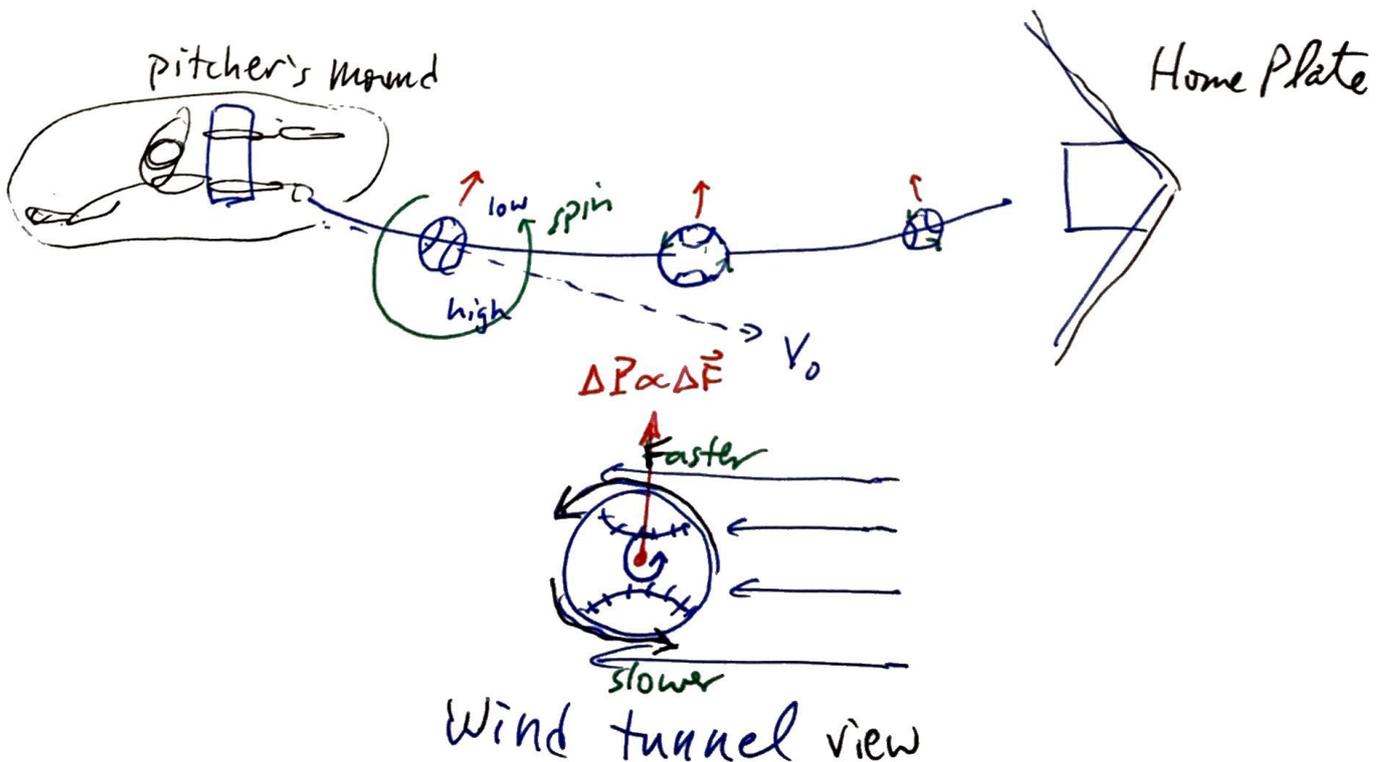
Faster flow lower pressures.

Vertically

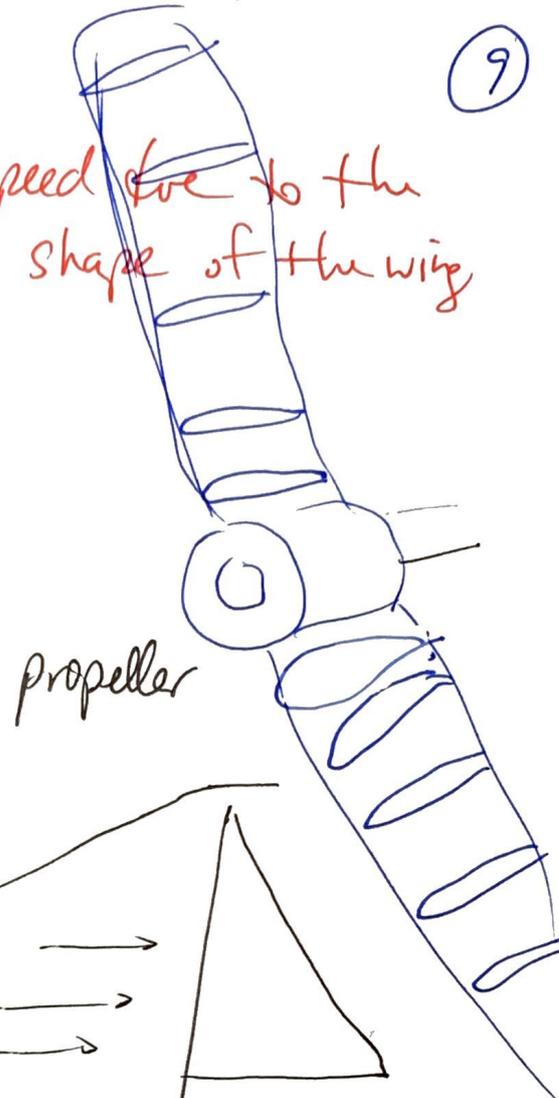
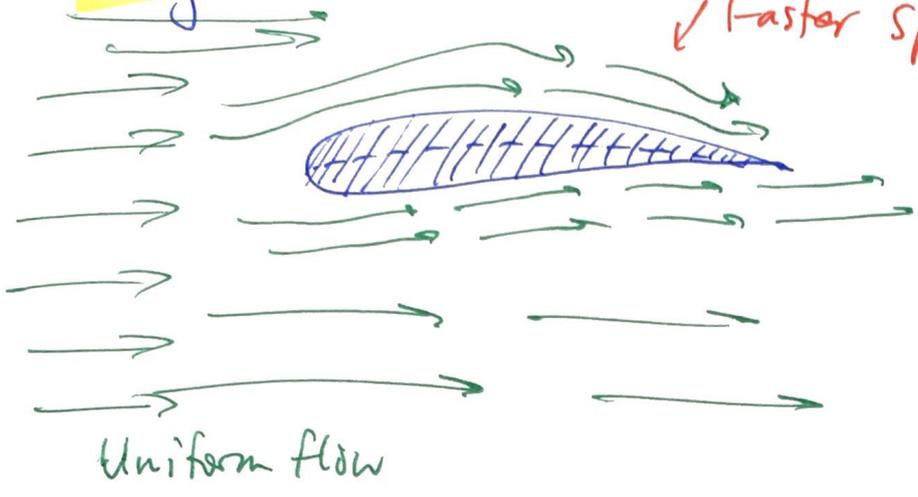


ping pong ball

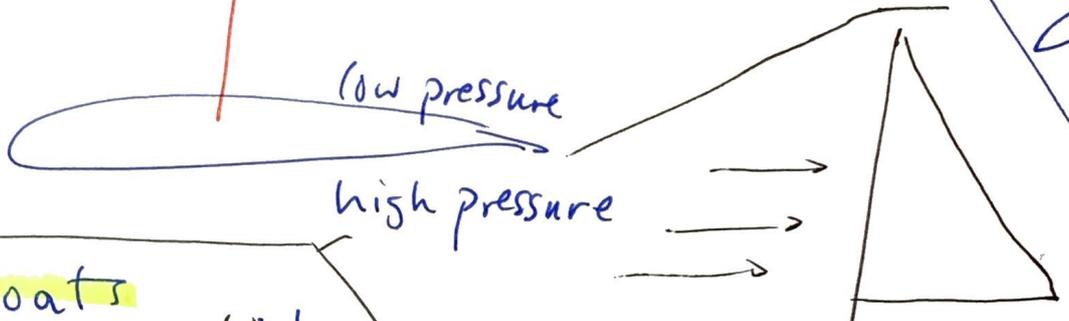
- curve pitches in baseball



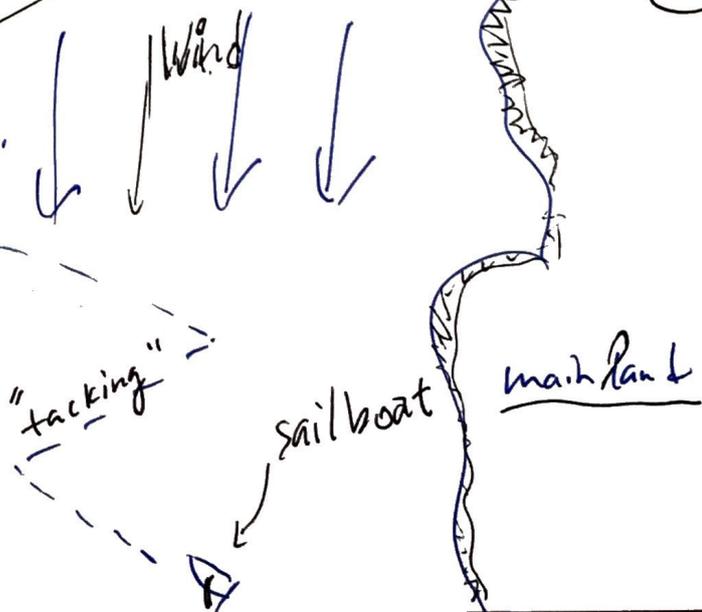
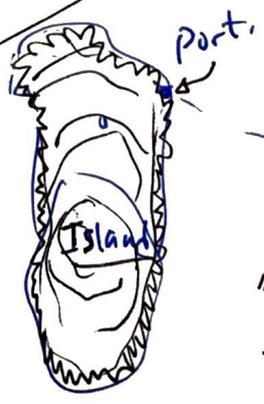
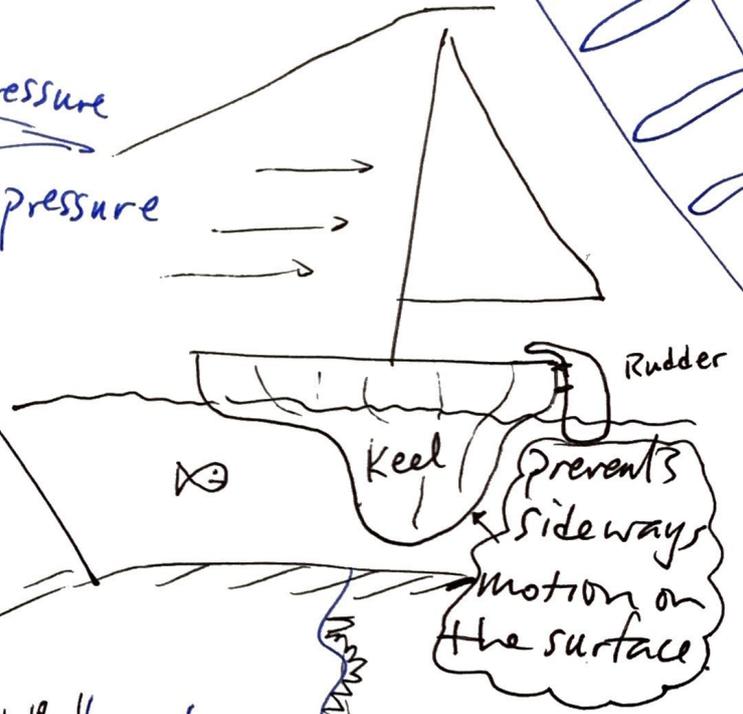
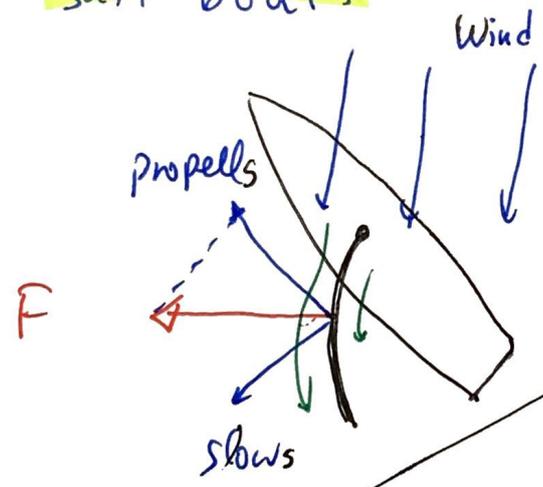
Wings and lift



Lift.



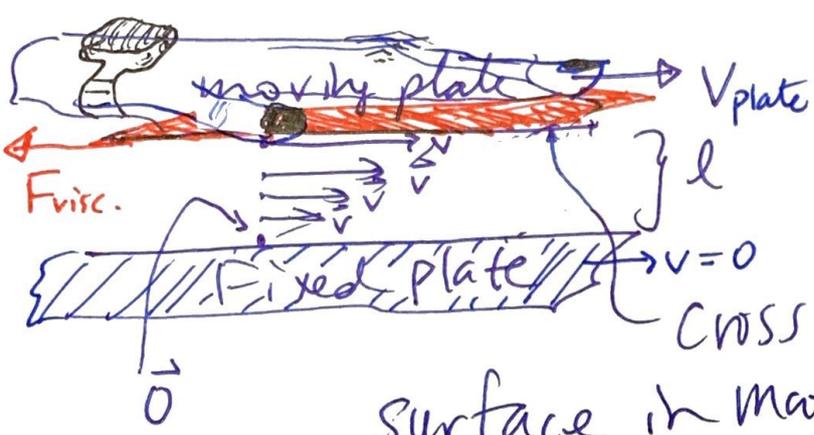
Sail boats



\* viscosity due to the friction of air molecules with themselves (their neighbors - "bonds")  
 the more dense a liquid the more viscous it tends to be.

$$F_{\text{drag}} = F_{\text{viscosity}} = \eta A \left( \frac{v}{l} \right)$$

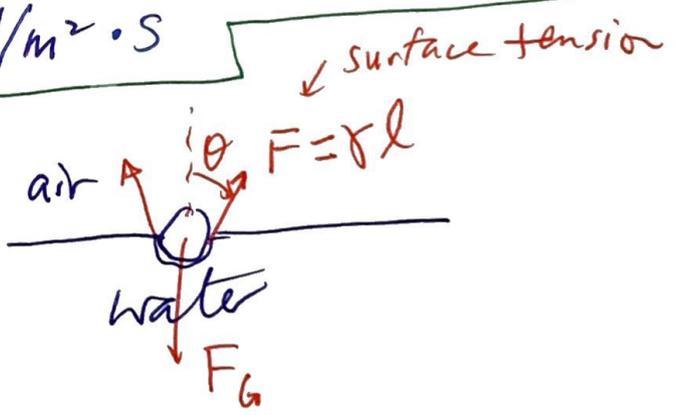
$\eta$  ← coefficient of viscosity  
 $A$  ← contact area  
 $v$  ← velocity of plate  
 $l$  ← channel width



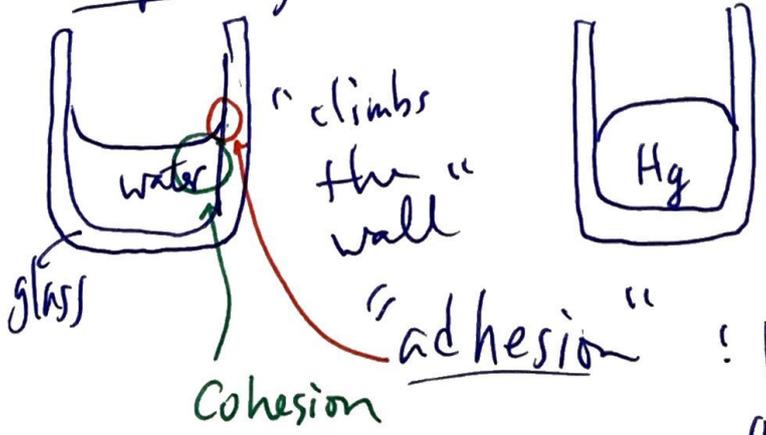
cross sectional area.  $A$  if surface in material contact to liquid.

$[\eta]$  Pa · s , N/m<sup>2</sup> · s

\* surface Tension



\* capillary Action



"Cohesion" Force between molecules of the same type

"adhesion" : Force between molecules of diff't types.